



gasoline



H2 always needs to be purified before use or re-use

\$110b of H2 made/yr

in plants making

fertilizer

chemicals





Two ways to purify H2 from "X"

- Chemical - Very high CAPEX - Complex
- + Simple
- + Scales all sizes

+ Good for massive scale + Can handle any gas composition Overkill for simple light gases **Normal Membranes (physical)** - Cannot handle acid gases (CO2, H2s) - Fouls (clogs) with heavy hydrocarbons (C₄+)

These shortcomings cause problems all over the H2 value chain

- Carbon Capture (CCUS) at H2 plants too expensive for almost a Gigaton of CO₂ (Blue H₂)

- Biomass Gasification limited in feasiblity (Green H2)

- Average refineries 'leaks' \$6m per year in H2 (Grey H2)

- Many other next-gen hydrogen projects have a bottleneck at separations as well

Enter Divigas

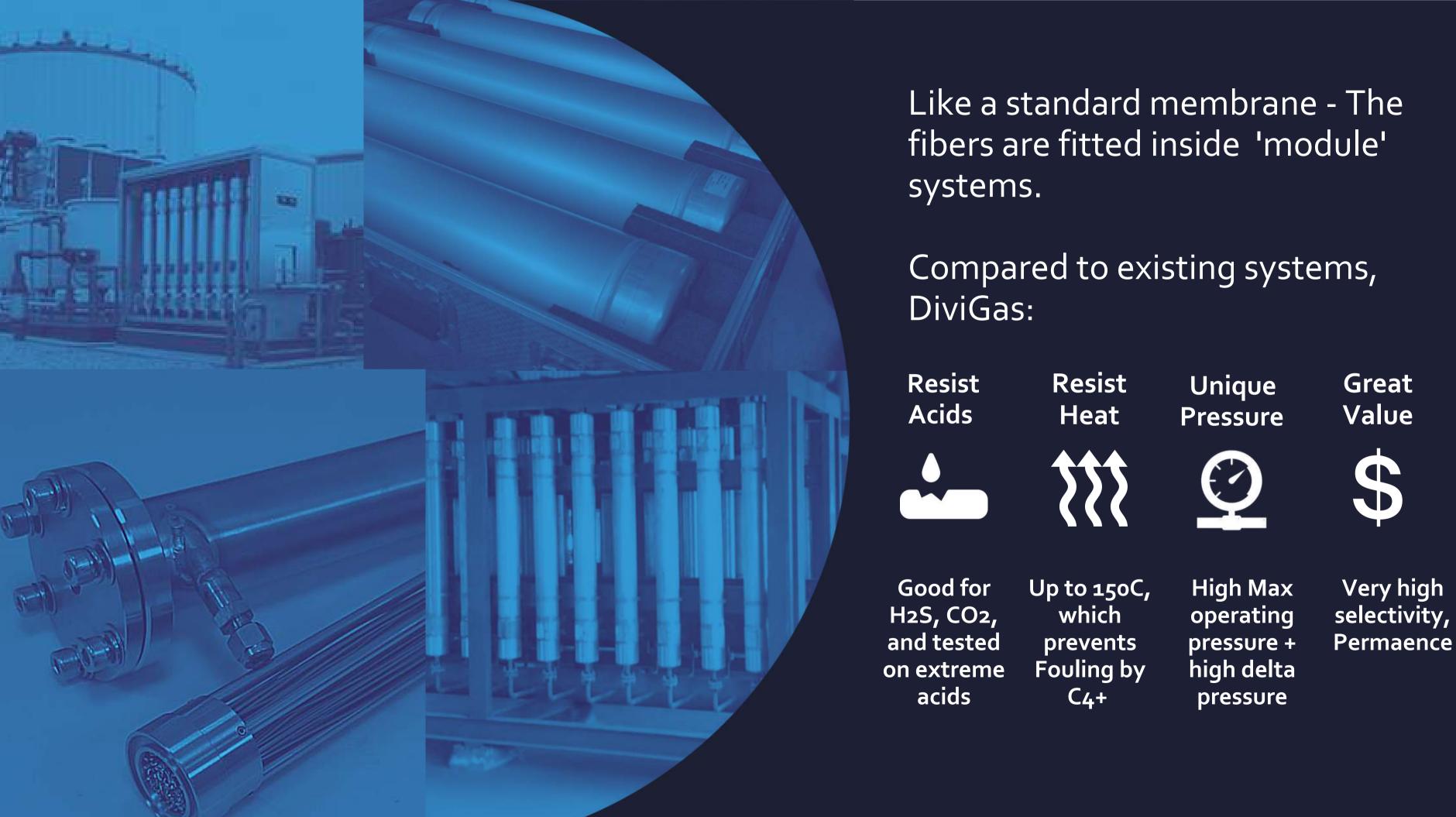
A proprietary new hollow fiber polymeric membrane that has resistant properties far beyond what is currently on the market at an affordable price



DIVI



10µm



Solved

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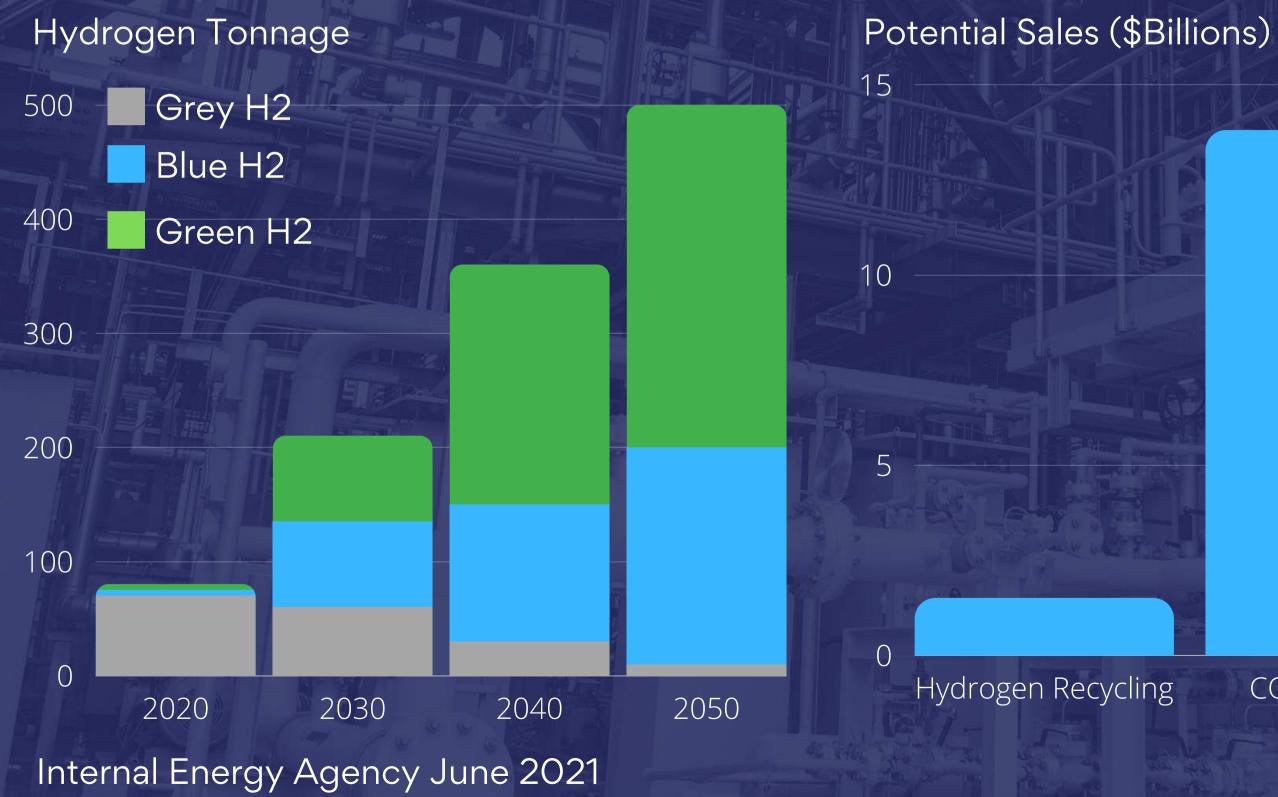
Key Differentiator

Resist Acid Resist U Heat Pr

: Unique Pressure Great Value







??\$B

CO2 Capture

Green H2 storage



2,000

1,500

1,000

500

WELLOW STATE

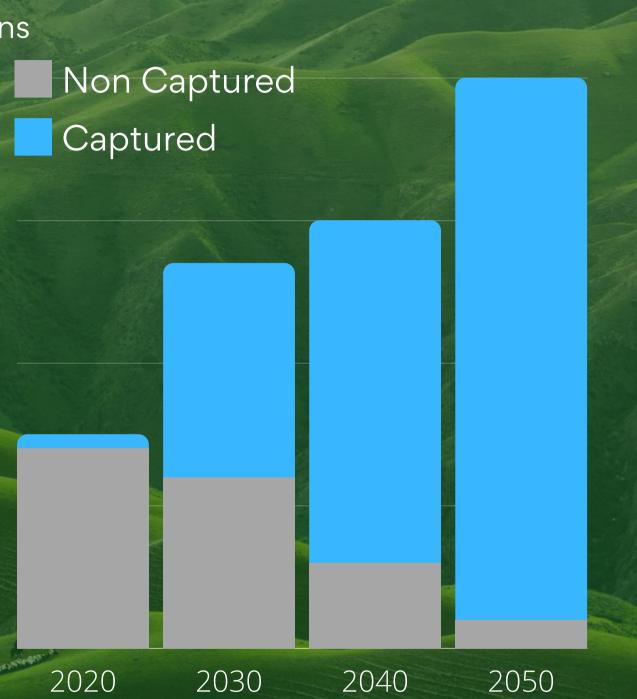
1 Ton of Grey H2 = ~10 Tons of CO2

Climate Impact

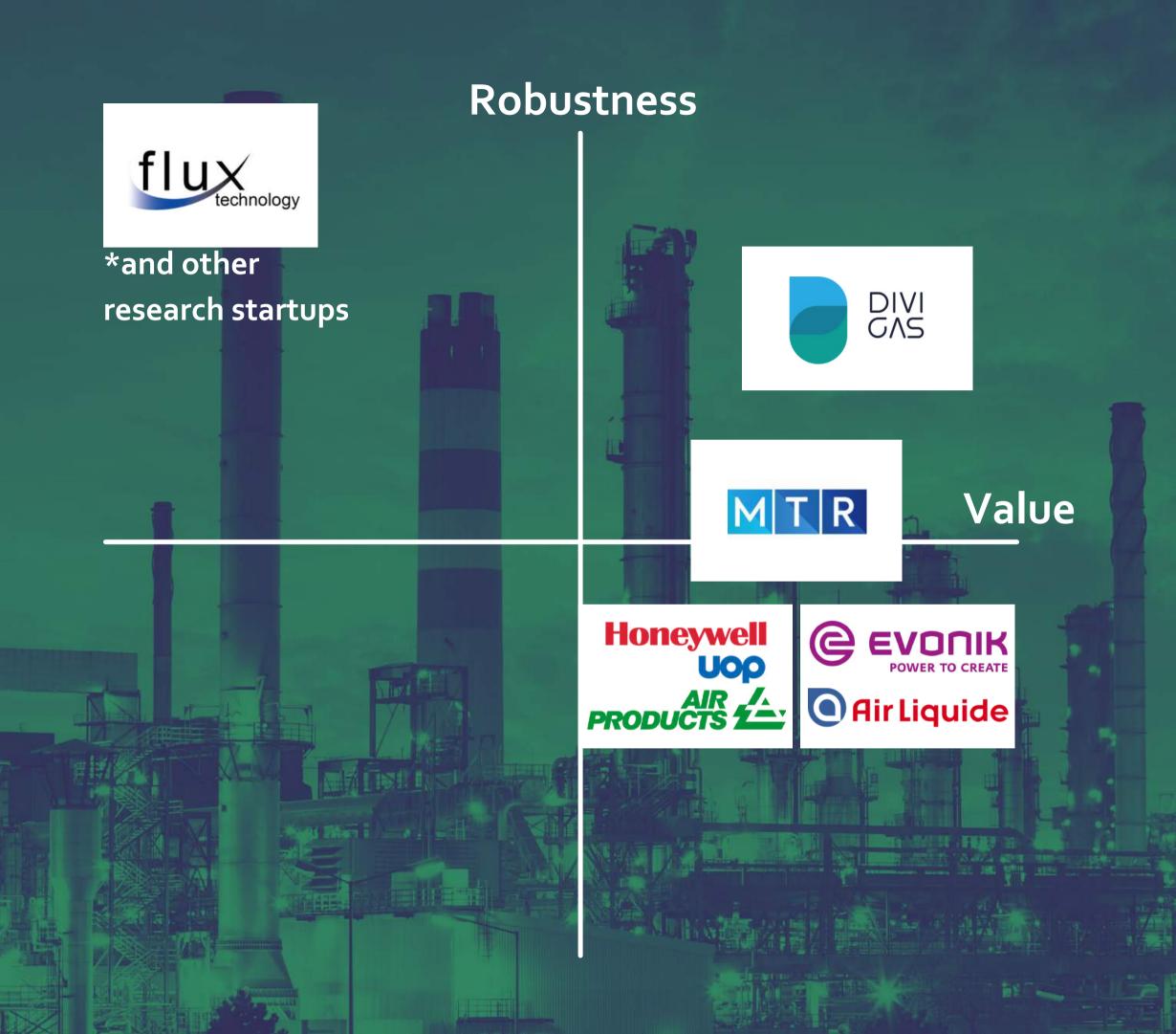
750 Million tons of CO2 made fromfossil fuel today2 Gigatons of CO2 by 2050

We can be a key piece of infrastructure for all of it

CO2 we could help sequester



IEA - "net-Zero by 2050" report from June 2021



DiviGas is the only membrane that - Is Affordable - Is Scalable - Can handle these difficult gases at high performance

Client Pipeline +08Clients Piloting

\$700K/yr Average Client size after pilot

• Our clients are large veteran equipment providers of refineries and plants

• They already approved price and performance and are waiting our pilots

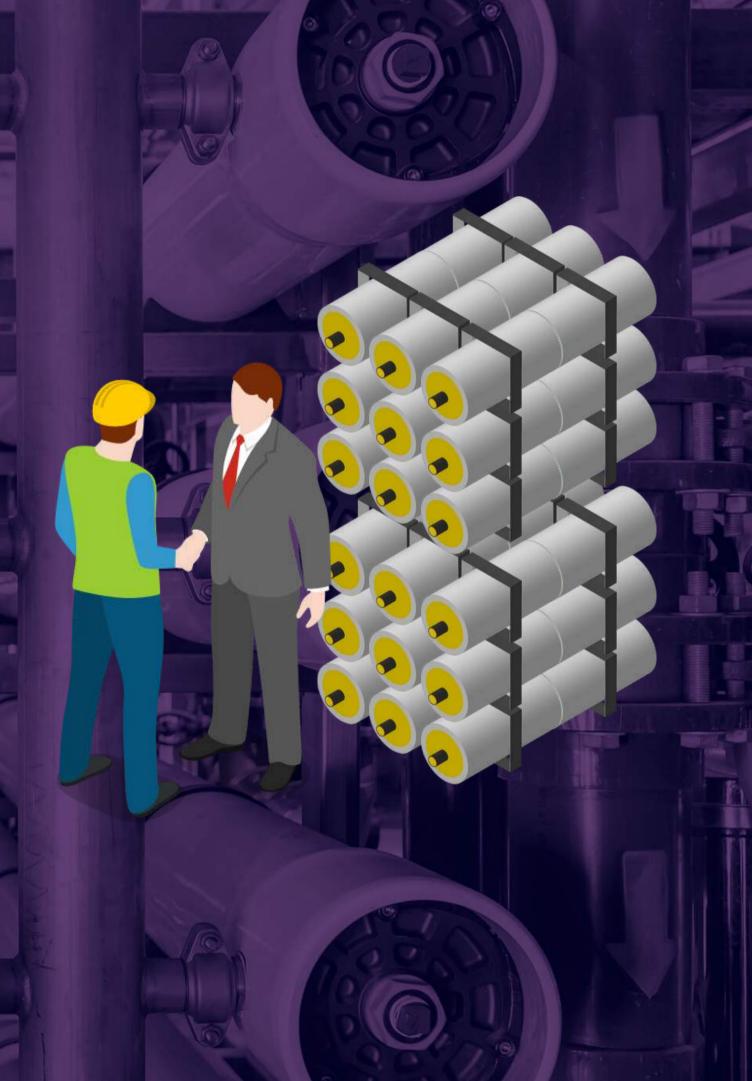
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>\$50M In pipeline

of clients Grey H2 Blue H2* Green H2 *overlap between Grey/Blue

Business Model

- Steel 'modules' systems sold to large plant equipment providers
 - Each module cost ~\$32,000
 - Any system can have 3-3000 modules
- Modules contain 'cartridges' that last 1-5 years before needing replacement
- System is guaranteed >15 years, deals (and revenues) locked in for decade+
- Clients can expect to save anywhere from \$60,000-\$100,000 per module or 2-3x their costs

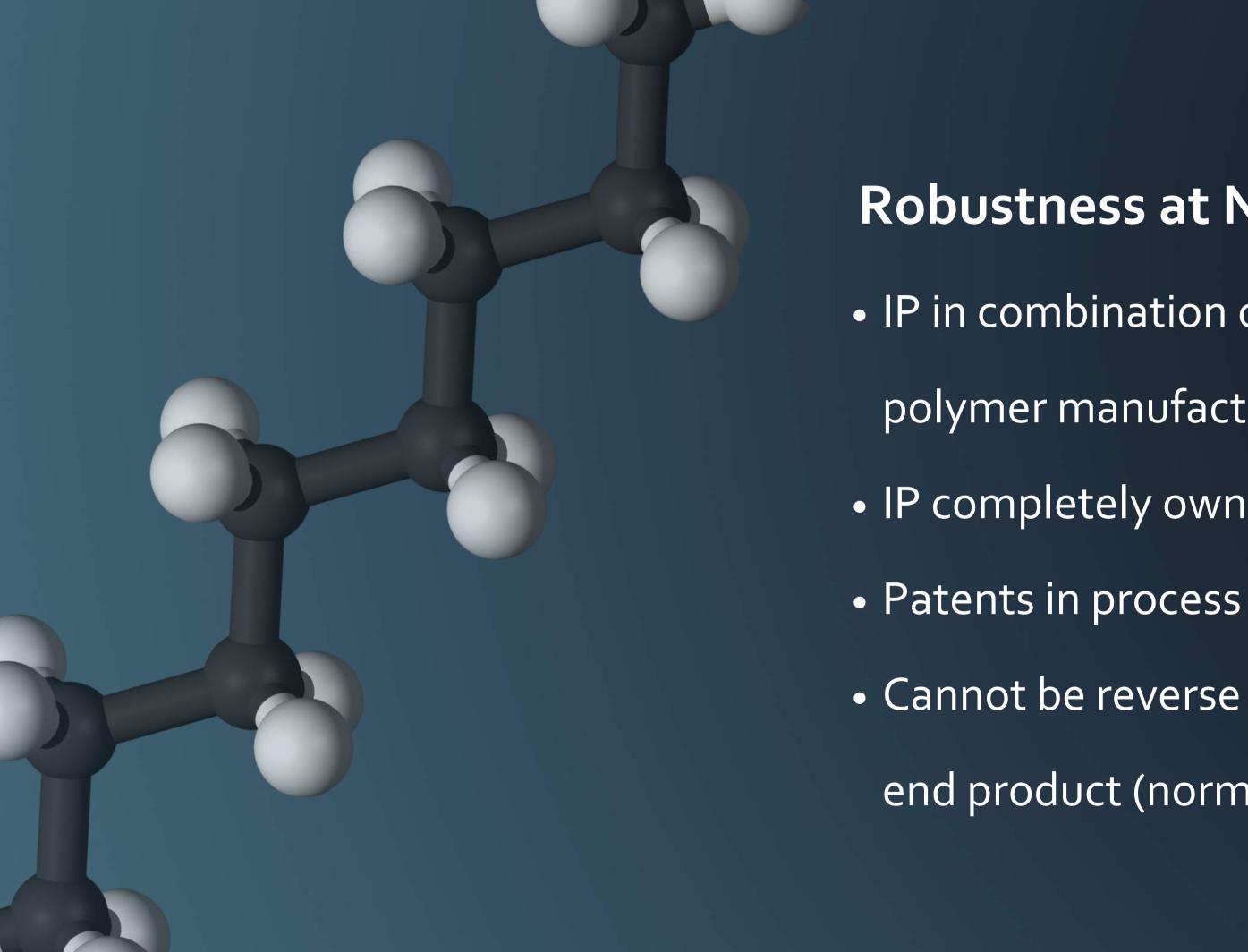


Dr. Ali Naderi CTO, Inventor & Cofounder

Discovered the idea for the uniquely strong polymer chain structure while patenting other membrane polymer tech with NUS for BASF. He realized its potential and started DIVIGAS

10 years of commercial work and research on polymers including on
Numerous membranes
Space shuttle ablative shielding
Car chassis crash dampening





Robustness at Nano-scale

- IP in combination of materials and
 - polymer manufacturing technique
- IP completely owned by DiviGas
- Cannot be reverse engineered from end product (normal for polymers)

What we've passed

Pre-Seed Round \$350K - POC

Lab Scale

Goal:

Prove end-product Obtain first clients

WHERE WE ARE

SEED ROUND \$3M - Industrial scale

First two mass manufacturing lines

Goal:

Field industrial scale rollouts \$Xm in recurring revenue

Where we are going

Growth Funding >\$10M - ScaleUp

Mass Scale Up

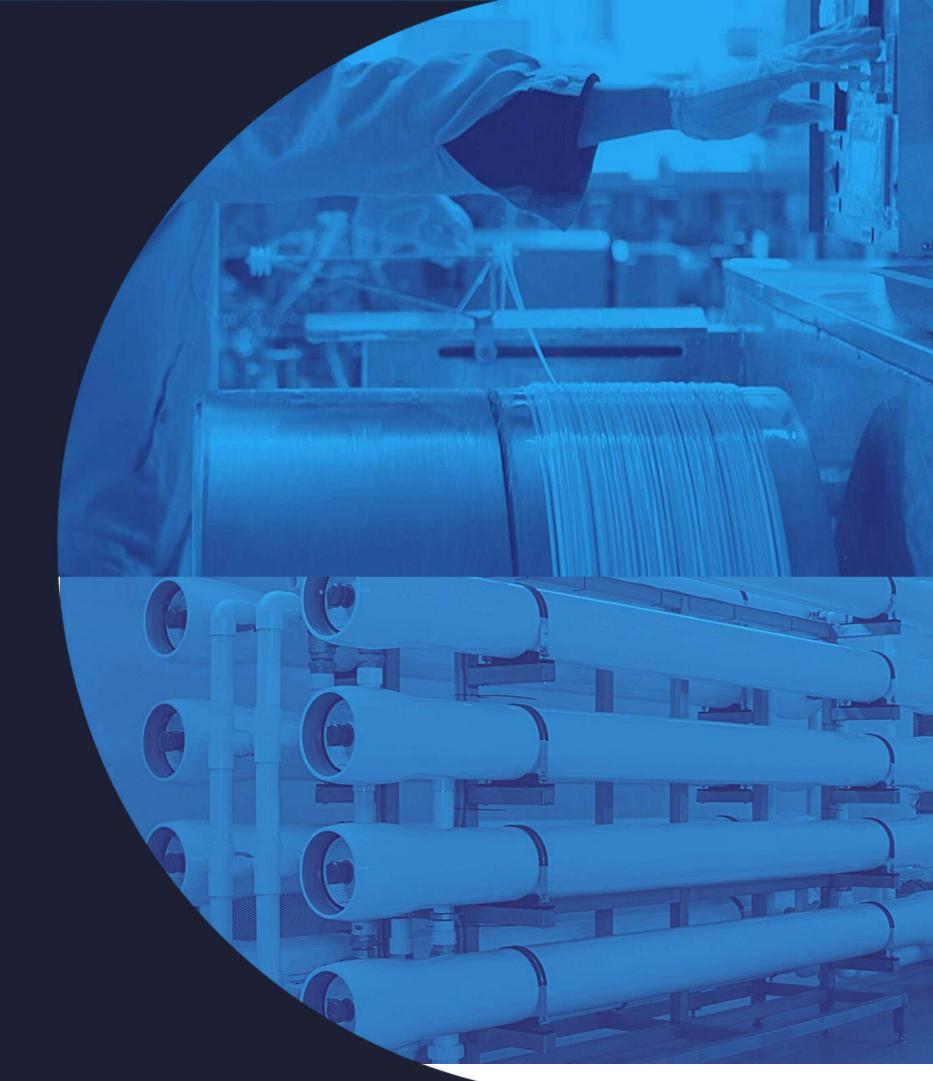
Goal:

Market-share dominance \$Xo-Xoom revenue

DIVI solution GAS DiviH

What this round takes us to:

- 2 manufacturing lines 70 modules per year total
- \$3m in potential revenue
 - Product Shipped, operating and outputting
 - Client demand for larger systems



André Lorenceau CEO & Founder

Repeat Founder, raised +\$15m Capital previously

Forbes 30under30

Led a team of 6o+ to deliver global media tech products

Funded and Backed by

HAX SUSV Em

Selected by and part of



Dr. Ali Naderi CTO & Founder

Master in Polymer Eng.

Ph.D. in Chemical Eng.

10 years of work and research experience on polymers

ALL SLIDES AFTER THIS ARE ANNEX

DIVI GAS

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Grey Hydrogen

What: Recycle wasted Hydrogen

Market: \$1-3B in membranes 6 Clients found

Why us: Tough gas handling

Where: Refineries PolyPropylene/Ethylene Nylon 6 plants

> Market stage: Mature

Use Cases

Blue Hydrogen

What: Carbon Capture at H2 plants

> Market: \$14B in membranes 2 Clients found

Why us: Co2 separation performance

> Where: Hydrogen plants

> > When: Emerging

Green Hydrogen

What: Green Hydrogen Energy Storage

Market: \$???B in membranes 2 Clients found

Why us: Co2 separation performance

> Where: H2 storage sites

> > When: Nascent

Multiple Potential on Seed in an Exit Scenario

we would not sell for less than \$100m

Bottom up analysis of market through one client that		All number	rs millions					
wants us to deliver >100 modules in 2023 Burns & Mcdonnel	Date	Stage	Revenue /yr	% of hydrotreat er market	Booked revenue	Valuation multiple (on Booked rev)	Exit price	Multiple on Seed (20% dil. per rd)
Type: Hydrotreater recovery \$3m /yr deal = \$45m in guaranteed/booked revenue		Seed	\$3.5	0.08%	\$52.5	2	\$105	8
over 15 yrs	2023-2024	Series A	\$20	0.44%	\$300	2	\$600	38
1 out of 6 refineries - 2 hydrotreaters per refinery. These 12 units could be worth \$36m a year, or \$540m guaranteed/booked revenue by 2024	2025-2026	Series B	\$75	1.67%	\$1,125	2	\$2,250	115
We already have 6 clients with similar use cases. Exit multiple (private or IPO) will not be on EBITDA but on market potential, booked revenue and clean impact. If we have \$150m in booked revenue in 2024,	There's 1500 hydrotreaters in the world. A potential of \$4.5b/yr in sale Il not be on EBITDA but on this use case alone, locked for 15 years for \$67.5b in total revenue venue and clean							

This is before smaller but very rapidly growing other markets - Other petrochemical Recovery (Likely another \$1b a year) - Carbon capture (another >\$10B/yr market) - H2-renewable energy storage (multiple \$B/yr market).

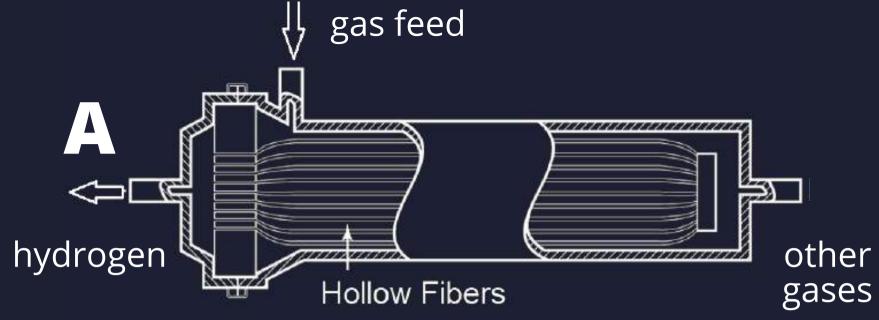
How it works - in detail

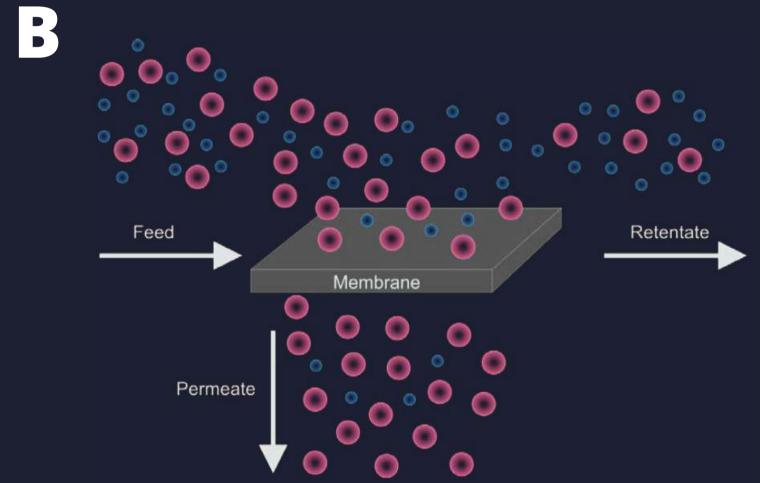
Mixed gas feed containing Hydrogen pushed through proprietary polymeric hollow fibers (A)

Pressure drives a molecular separation of the Hydrogen only (B) - <u>See video here</u>

Pure Hydrogen comes out at slightly lower pressure

Other Gases (such as CO₂) come out together at full pressure

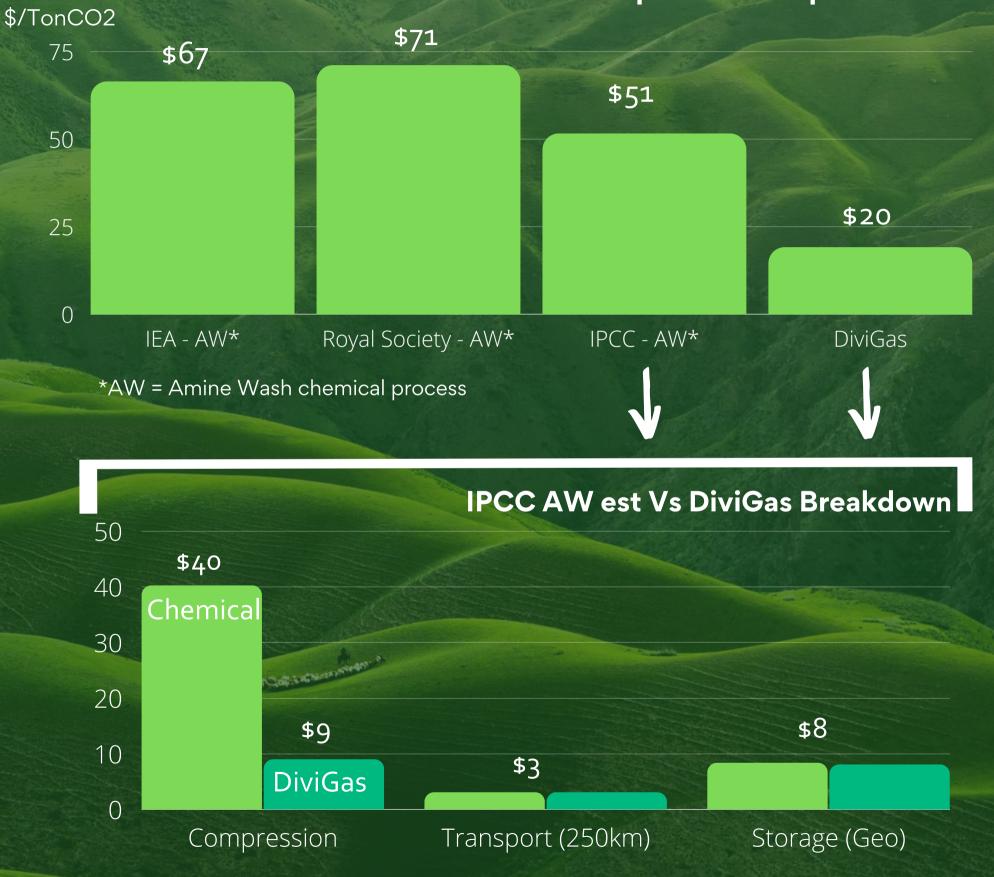


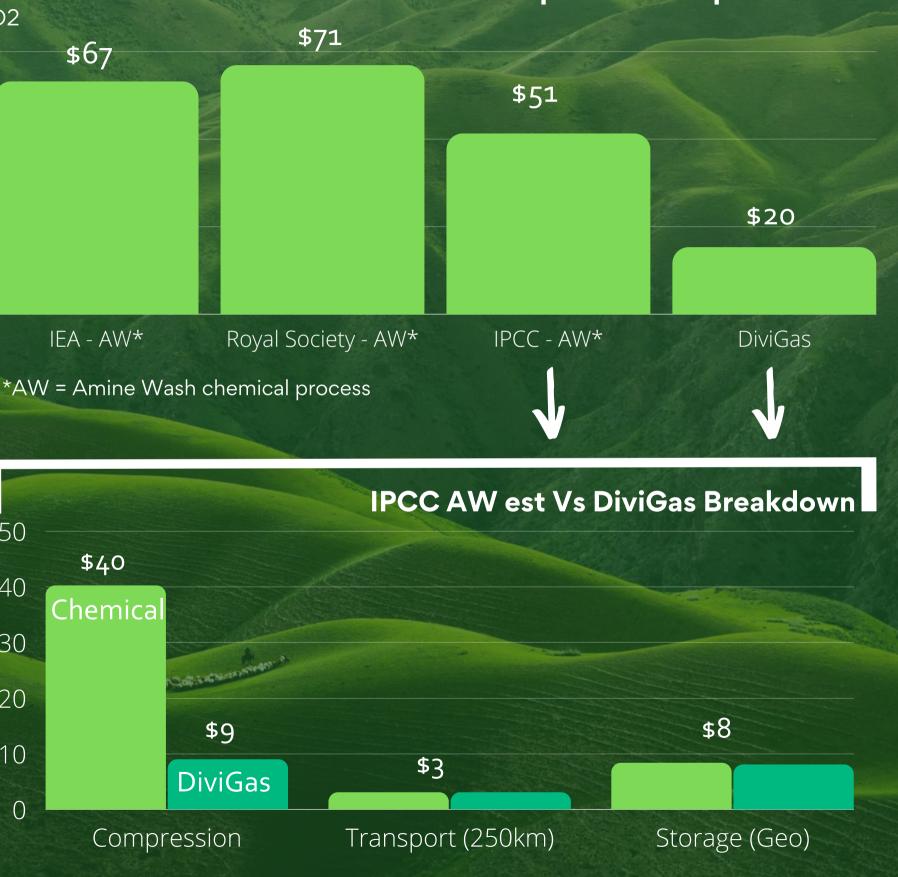


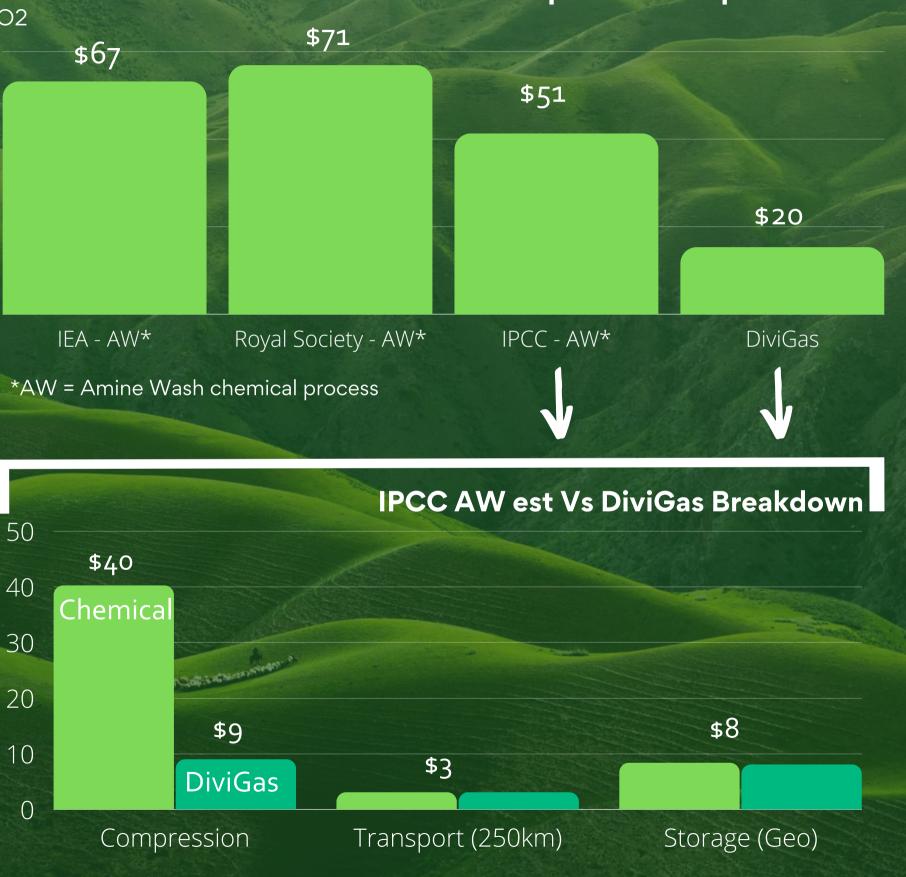
Carbon Capture (CCUS) Economics

For Carbon Capture, a huge portion of the cost is in compression of CO2 after separation

Our membrane is the only one that can separate pure CO₂ from H₂ at full pressure, dramatically reducing CCUS costs by removing compression needs







Carbon Capture Costs per Tech

Carbon Capture (CCUS) Economics III - Carbon Taxes

A number of laws today give tax breaks or price each ton of CO2 emitted.

At \$50/CO2ton, already existing in the US and multiple countries our technology, (as show on the right), would save \$30 per ton of CO2, and since H2 produces ~10 CO2 weight per H2, we save \$300 in credits per ton of H2 separated

- Significant Existing laws to price CO2
 - US '45Q' ~\$50/ton tax credit
 - France ~\$49/ton tax
 - Sweden ~\$119/ton tax
 - EU (ETS) ~\$19/ton (world bank)
 - And many more

• Incoming Laws

- EU Covid package (30% for climate, June 2021)
- Chinese 2030 neutrality plan (est 2021)
- Biden US Climate package (est 2021)
- Japan Carbon tax upgrade (est 2021)
- Korea Carbon tax upgrade (est 2021)

75

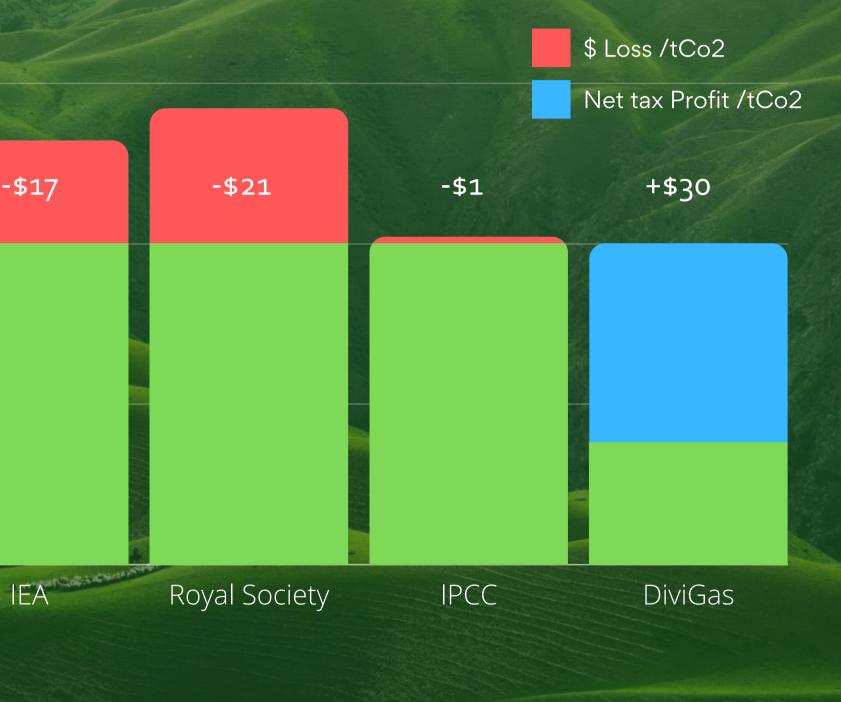
50

25

-\$17



Net Profit/Deficit /TonCo2 under current US tax credit "45Q"



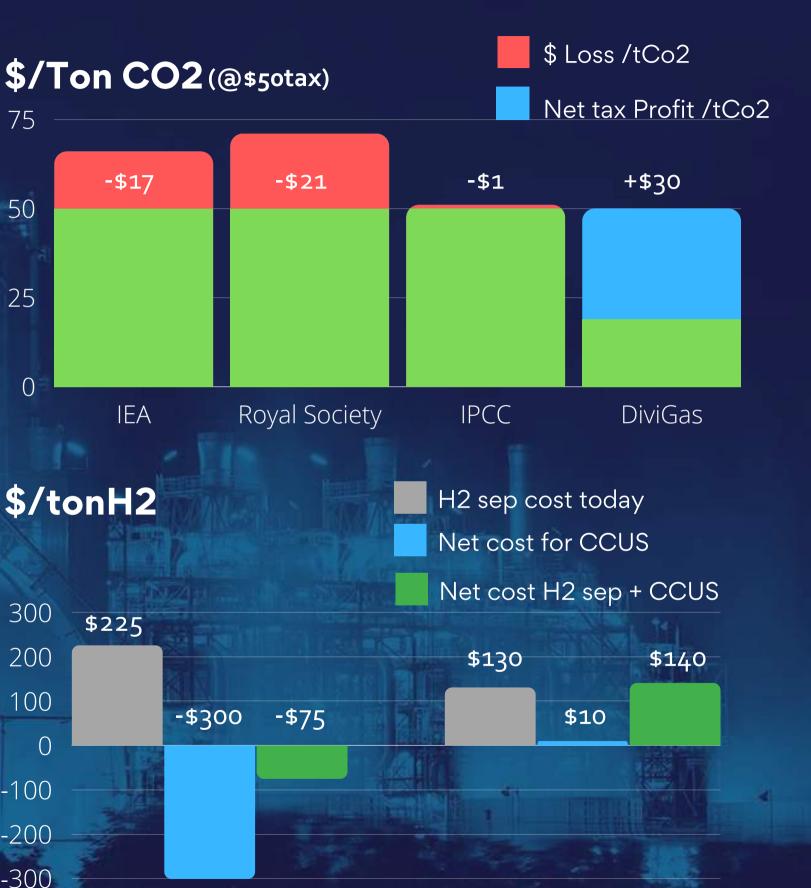
Carbon Capture (CCUS) Economics II

Today making 1 ton of hydrogen makes 10 ton of CO2 costing a total of \$130 (without CCUS)

Under "45Q", the \$50/tonCo2 tax credit, DiviGas CO2 capture would create a \$300 of tax credit per ton of H₂, resulting in a total of \$75 in profit /tonH2, before even selling/using the H2

For more math on the topic, check out our 3 in depth annex slides

Cost Of H2 separation with/without CCUS



DiviGas CCUS

75

50

25

0

300

200

100

-100

-200

-300

 $\left(\right)$

Chemical CCUS (IPCC)

Theoratical SMR CCUS Stream

SMR			
Purity%	99.00%		
Recovery%	95%		

	Inlet (SM1) % MOLE	Kmol/hr	Mass (Kg/hour)
TOT	100%	201.716	2100
H2	80%	161.4	325.3
CO2	20%	40.3	1775.5
	Temp		150
	Pressure		60

Number of module total	
Stage 1	
Stage 2	

	Post Membrane (SM2)			
	% MOLE	Kmol/hr	Kg/hour	
TOT	100%	152	321	
H2	99.0%	152	304	
CO2	1.0%	0.40343	17.75092	
	Temp		150	
	Pressure		45	

		Residue 1 (SM % MOLE	Kmol/hr	Kg/hour
	TOT	100%	6 49.5	1777
\rightarrow	H2	19%	6 9.6	19
0.500	CO2	81%	39.9	1757.3
		Temp		150
		Pressure		60

